

## PHENOL DEGRADATION ON GLASS FIBRES WITH IMMOBILIZED TITANIUM DIOXIDE PARTICLES

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The photocatalytic mineralization of phenol in aqueous solutions under various experimental conditions was employed, to test the activity of the prepared immobilized fibreglass/TiO<sub>2</sub> photocatalysts. The particles of titanium dioxide P25 were coated on the surface of commercial fibreglass fabric by dipping in ethanolic TiO<sub>2</sub> suspensions and were fixed by firing 6 h at 500 °C.

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The photocatalytic water purification on the irradiated titanium dioxide surface in the presence of oxygen is very effective process resulting in the complete mineralization of organic pollutants<sup>1</sup>. Recently the attention is especially focused on the degradation of phenols and phenol derivatives in TiO<sub>2</sub> aqueous suspensions<sup>2-13</sup>. The photocatalytic mineralization of organic substrates in aqueous titanium dioxide suspensions is very efficient. These systems, however, require the pretentious removing of TiO<sub>2</sub> particles from the solutions. Thus the technological utilization of photocatalytic processes for water purification demands the fixation or preparation of active TiO<sub>2</sub> surface on the suitable supporting materials<sup>1</sup>. The thin TiO<sub>2</sub> films were prepared on the glass wall of photoreactors by dipping in TiO<sub>2</sub> suspensions<sup>14,15</sup> or the particles of active TiO<sub>2</sub> were fixed on the sand by heating at 400 °C (ref.<sup>16</sup>). The immobilized TiO<sub>2</sub> particulate films were produced from suspensions on an optically transparent electrode<sup>17</sup>. The fixed titanium dioxide layers may be obtained also by the anodic oxidation<sup>18</sup>, by the oxidation in plasma<sup>19</sup> or by electron-beam evaporation<sup>20</sup>. Sol-gel techniques were employed to coat the glass supports with colloidal solutions, subsequent firing leads to the formation of photocatalytic TiO<sub>2</sub> ceramic membranes<sup>21,22</sup>. The firing temperature dominantly determines the structure of TiO<sub>2</sub>; the temperature below 600 °C guarantees the formation of active anatase structure<sup>23,24</sup>.

## EXPERIMENTAL

Phenol, (Reactivul, Romania) was used without further purification. All the chemicals were of analytical grade purity. The commercial fibreglass fabric V 131350/651 (Skloplast, The Slovak Republic) was applied as the supporting material for the titanium dioxide P25 particles (Degussa, Germany) immobilization. The fundamental properties of the glass fabric were: thickness, 0.4 mm; fibre diameter, 13  $\mu\text{m}$ ; surface weight, 350  $\text{g m}^{-2}$ ; coating material, methacryl silane.

After removal of the coating material from the technical fibreglass fabric by firing at 400  $^{\circ}\text{C}$  for 4 h, the fabric was coated by titanium dioxide particles. The glass fibres were dipped into  $\text{TiO}_2$  suspension ( $\text{TiO}_2$  concentration 5  $\text{g l}^{-1}$ ) in ethanol and the dried composition was calcinated 6 h at 500  $^{\circ}\text{C}$ . Non-fixed particles were removed from the surface by rewashing in water.  $\text{TiO}_2$  particles fixation was sufficiently stable, the particles remained at the surface of the fibreglass even in a common aqueous ultrasonic bath. The concentration of supported  $\text{TiO}_2$  was determined by measuring the turbidity ( $\lambda$  530 nm) of the suspension obtained by removing the  $\text{TiO}_2$  particles from fibreglass fabrics (2 h sonification in concentrated  $\text{H}_2\text{SO}_4$  was the only successful method of the particles removing).

The photocatalytic activity of  $\text{TiO}_2$  immobilized on glass fibres (area 1  $\text{dm}^2$ ) was tested in the phenol degradation reaction. The photoreactions (sample volume 130 ml) were carried out in a photochemical immersion well (Applied Photophysics, United Kingdom) using a Pyrex sleeve for cutting out the radiation below 300 nm and for inhibiting any direct photochemical transformations of phenol. A 125 W medium-pressure mercury lamp (Applied Photophysics, United Kingdom) inserted in the central part of photoreactor was employed as a radiation source. The irradiated systems were continuously saturated by dioxygen during the exposure (flow rate 200  $\text{ml min}^{-1}$ ).

The photoexperiments with the circulating phenol solutions (sample volume 300 ml) were performed in a flat photoreactor with Pyrex window (area 1  $\text{dm}^2$ ) irradiated by the external radiation source (400 W medium-pressure mercury lamp RWL, Tesla, The Czech Republic). Under these experimental conditions the prepared phenol solutions were saturated by dioxygen (flow rate 200  $\text{ml min}^{-1}$ ) in the stock vessel outside of the active irradiated zone of photoreactor.

The phenol concentration in the samples was determined by HPLC (FPLC Pharmacia, Sweden) using a Separon SIX C-18 column (Tessek, The Czech Republic) and UV detector ( $\lambda$  280 nm). The mixture of methanol–water– $\text{H}_3\text{PO}_4$  (35 : 65 : 0.1) was applied as a mobile phase.

The reflectance spectra of titanium dioxide samples were measured using UV-VIS spectrophotometer (M40, Zeiss, Germany) equipped with a reflectance accessory with an integration sphere. The UV-VIS spectra of solutions and their turbidity were measured on Philips UV-VIS spectrophotometer PU 8800 in cell path of 0.2 and 1 cm, respectively. The scanning electron microscopy of fibreglass samples was performed by Jeol JXA-840 A analyzer.

## RESULTS AND DISCUSSION

The above described procedure of  $\text{TiO}_2$  particles deposition on glass fibres results in preparation of immobilized layers characterized by titanium dioxide concentration of 6 mg per 1 g of fibreglass. The glass fibres obtained by scanning electron microscopy before (a) and after (b) titanium dioxide deposition are depicted in Fig. 1.

The normalized reflectance spectra of  $\text{TiO}_2$  P25 powder (80% anatase, 20% rutile)<sup>11</sup>, glass fibres with deposited  $\text{TiO}_2$ , and rutile powder are shown in Fig. 2. The obtained reflectance spectra confirmed only negligible transformation of P25 to rutile structure by calcination (6 h at 500  $^{\circ}\text{C}$ ).

Rapid decrease of phenol concentration in aqueous solutions during irradiation at various temperatures using  $\text{TiO}_2$  immobilized on glass fibres is illustrated in Fig. 3. The dependence of phenol concentration on the irradiation time was successfully fitted (by the non-linear least squares minimization procedure) to an exponential function using program SCIENTIST (MicroMath). Formal first-order kinetics were proposed for phenol decomposition and the formal first-order rate constants were evaluated. From these the phenol half-times,  $\tau_{0,5}$ , in experimental systems were calculated<sup>25</sup>. The obtained values of phenol half-time were used for the comparison of the efficiency of the photocatalytic process under different reaction conditions.

The release of  $\text{TiO}_2$  particles from the fibreglass support by manipulation and/or irradiation was not observed, the solutions remained transparent all the time and no turbidity was measured in UV spectra as shown in Fig. 4. Consequently the stability of the fibreglass/ $\text{TiO}_2$  photocatalyst was sufficient, but surprisingly the phenol half-times became longer and longer during the repeated degradation experiments (16 cycles of 90 min exposure) as depicted in Fig. 5. The decrease of photodegradation activity is significant after 20 h irradiation. We were extensively looking for the reason of such activity decrease, and we found that during the exposure the  $\text{TiO}_2$  surface is saturated by adsorbed intermediates

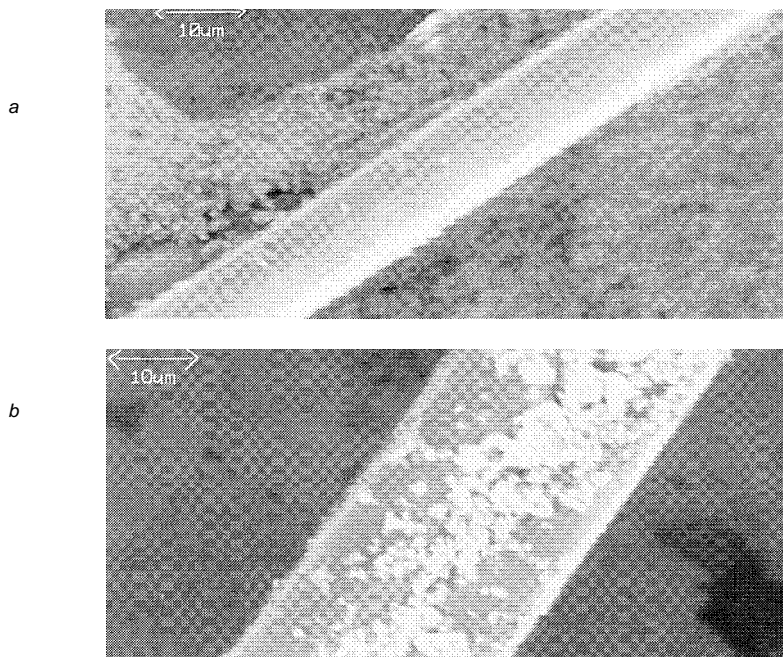


FIG. 1

Scanning electron microscopy of the glass fibres before (a) and after (b) surface deposition of  $\text{TiO}_2$

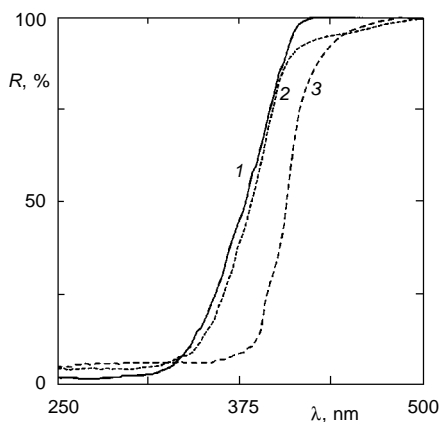


FIG. 2

The reflectance ( $R$ ) spectra of  $\text{TiO}_2$  P25 powder (1), glass fibres with  $\text{TiO}_2$  deposited by calcination at  $500^\circ\text{C}$  (2) and powder rutile (3)

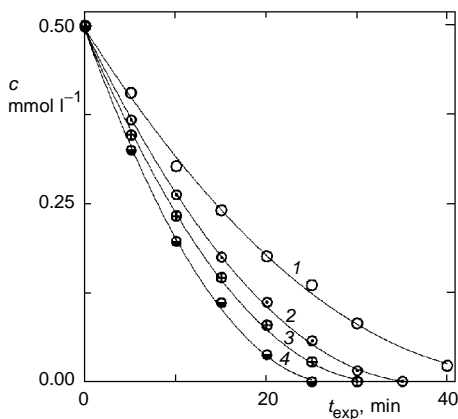


FIG. 3

The dependence of phenol concentration ( $c$ ) on the irradiation time ( $t_{\text{ext}}$ ) at various temperatures using  $\text{TiO}_2$  supported on glass fibres;  $c_0$   $0.5 \text{ mmol l}^{-1}$ . Temperature ( $^\circ\text{C}$ ): 1 30, 2 40, 3 50, 4 60

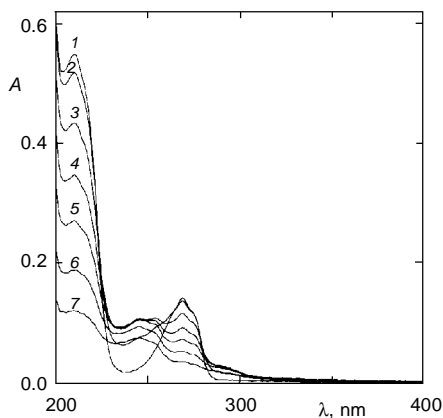


FIG. 4

Changes of absorption ( $A$ ) in UV spectra in dependence on the time of irradiation in the phenol aqueous system using  $\text{TiO}_2$  supported on glass fibres;  $c_0$   $0.5 \text{ mmol l}^{-1}$ , cell  $0.2 \text{ cm}$ . Exposure (min): 1 0, 2 5, 3 10, 4 15, 5 20, 6 25, 7 30

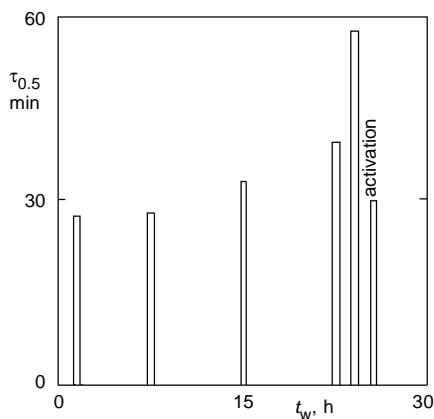


FIG. 5

The dependence of phenol half-time ( $\tau_{0.5}$ ) on the working time ( $\tau_w$ ) of fibreglass/ $\text{TiO}_2$  photocatalyst ( $c_0$   $1 \text{ mmol l}^{-1}$ , temperature  $25^\circ\text{C}$ )

of phenol degradation, e.g. hydroquinone and catechol<sup>7</sup>. (The formation of these intermediates was monitored in our experiments by HPLC). After removing the adsorbates from the TiO<sub>2</sub> surface by heating (2 h at 200 °C) or by irradiation in the acidic aqueous solution ( $c_{\text{HCl}}$  1 mmol l<sup>-1</sup>), the fibreglass/TiO<sub>2</sub> photocatalyst recover again the primary activity (Fig. 5). If the total working time of fibreglass/TiO<sub>2</sub> photocatalysts,  $t_w$ , remains below 15 h, its reactivating is not necessary.

The linear dependence of phenol half-times on the initial concentration of phenol,  $c_0$ , is illustrated in Fig. 6. Such kinetic behaviour is characteristic for Langmuir–Hinshelwood description of the surface photocatalytic reactions in systems with constant dioxygen concentration as described in the equation<sup>22</sup>

$$\tau_{0.5} = \frac{\ln 2}{k_1} + \frac{K_{\text{ph}}}{2k_1k_2} c_0, \quad (1)$$

where  $K_{\text{ph}}$  is the adsorption constant of phenol,  $k_1$  and  $k_2$  are formal experimental constants including the influence of experimental arrangement and the dioxygen concentration<sup>22</sup>.

From the least-squares analysis of the data shown in Fig. 6 (intercept 4.0 min, slope 25.7 min l mmol<sup>-1</sup>, R squared 0.98) we evaluated the phenol adsorption constant  $K_{\text{ph}} = 8.9$  l mmol<sup>-1</sup>. This value may be compared with adsorption constant  $K_{\text{ph}} = 4.07$  l mmol<sup>-1</sup> reported for phenol decomposition in aqueous titanium dioxide suspension<sup>2</sup>.

The temperature dependence of phenol decomposition rate was investigated in the range 25 – 60 °C. This dependence can be formally described using Arrhenius equation<sup>15,26</sup>

$$\tau_{0.5} = A \exp\left(-\frac{E_a}{RT}\right), \quad (2)$$

where  $A$  is a constant, and  $E_a$  is the apparent activation energy of the photocatalytic process.

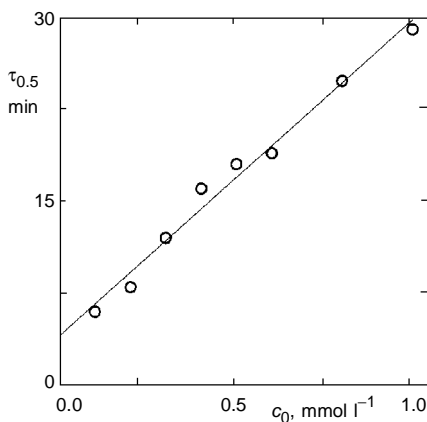


FIG. 6  
The dependence of phenol half-time ( $\tau_{0.5}$ ) on the initial phenol concentration ( $c_0$ ) (dioxygen saturated systems, temperature 25 °C)

The apparent activation energy of the phenol decomposition can be calculated from the slope of the linearized Eq. (2) after least-squares analysis. Figure 7 illustrates such Arrhenius plot for the temperature dependence of phenol half-times (slope 1 765 K, R squared 0.96). The calculated value of the apparent activation energy of phenol degradation on irradiated fibreglass/TiO<sub>2</sub> is of 14.7 kJ mol<sup>-1</sup> and is in a good agreement with activation energies obtained for phenol removal on immobilized TiO<sub>2</sub> layer by Matthews<sup>15</sup> and Okamoto<sup>26</sup>.

The positive effect of higher temperature on the phenol degradation rate can be explained under assumption that the increase in temperature improve the photoreaction to compete with electron-hole recombination process<sup>27</sup>. The rate of formation electron-hole pairs depends also upon the temperature of semiconductor controlling its Fermi band position<sup>28</sup>. The increase in temperature may also increase the desorption of physisorbed species from the irradiated surface<sup>29</sup>.

The study of the fibreglass/TiO<sub>2</sub> immobilized systems with circulated pollutant solution is necessary for the applications of photocatalytic processes of water purification in the future. The dependence of the phenol half-times on the flow rate of solution,  $q$ , through the active zone of photoreactor with external dioxygen saturation and irradiation source, is depicted in Fig. 8. The results showed the significant decrease in the phenol degradation half-time with increasing flow rate, confirming mass transfer limitations in accordance with other studies with immobilized TiO<sub>2</sub> photocatalysts<sup>16,30</sup>.

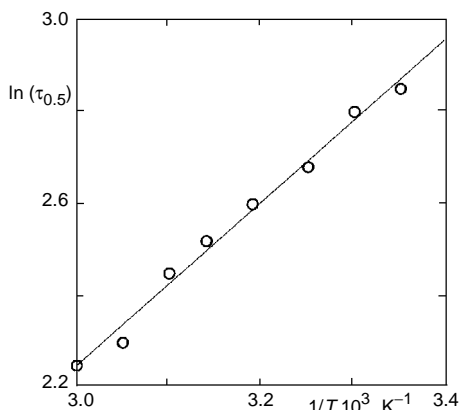


FIG. 7

The Arrhenius analysis of the dependence of phenol half-time on temperature (dioxygen saturated systems,  $c_0$  0.5 mmol l<sup>-1</sup>)

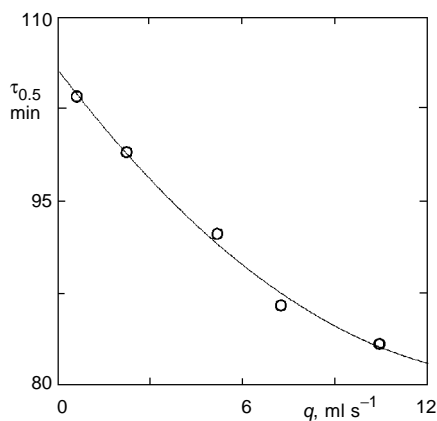


FIG. 8

The dependence of phenol half-times ( $\tau_{0.5}$ ) on the flow rate ( $q$ ) of solution through the active zone of flat photochemical reactor ( $c_0$  1 mmol l<sup>-1</sup>, temperature 25 °C)

The active titanium dioxide particles were fixed on the commercial glass fibres by very simple procedure. The removing of  $\text{TiO}_2$  from the prepared fibreglass/ $\text{TiO}_2$  photocatalyst during irradiation in aqueous solutions was fully inhibited. The immobilized photocatalysts were tested in reaction of phenol decomposition in aqueous solutions under various experimental conditions.

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